

**Research article**

## **Extraction of bioactive compounds from yerba mate (*Ilex paraguariensis* St.-Hil.) leaves by packed-bed extractor using hot water as solvents: Kinetics study and mathematical modeling**

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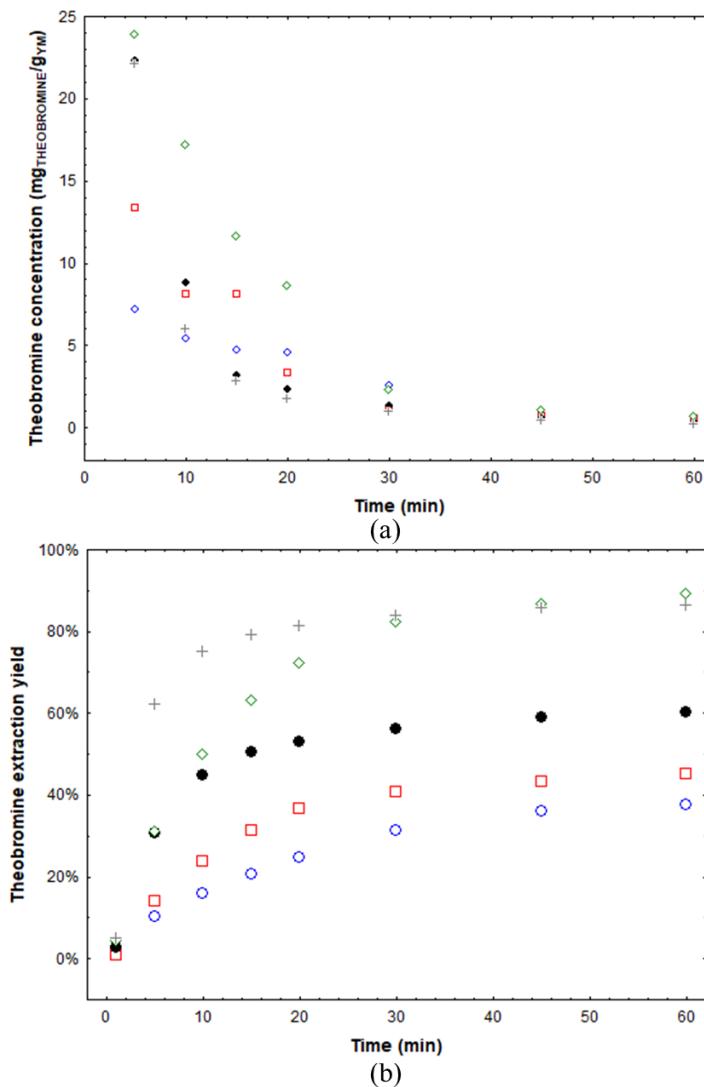
## Supplementary file

**Table S1.** Statistical analysis of bioactive compounds extraction from yerba mate using central composite design (CCD)\*.

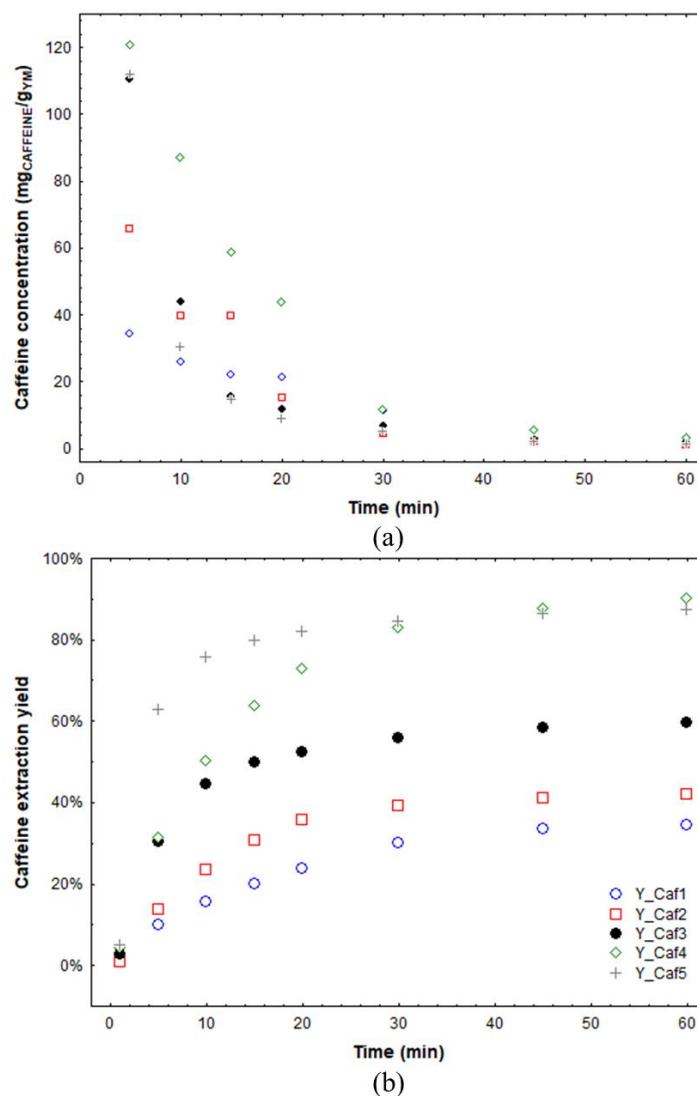
Parameters	Effect	Std. Err.	Coeff.	Std. Err. Coeff	p**
<b>Total phenolic content (TFC)</b>					
Mean	760.36	4.31	760.87	4.31	$2.46 \times 10^{-20}$
Temperature (1)	541.75	9.64	520.52	4.82	$7.03 \times 10^{-15}$
Feed flow rate (2)	24.09	9.64	2.86	4.82	0.03
1by2	-67.26	9.64	-88.49	4.82	$2.30 \times 10^{-5}$
<b>Theobromine</b>					
Mean	37.04	0.41	37.04	0.41	$3.20 \times 10^{-17}$
Temperature (1)	29.46	0.92	14.73	0.46	$3.20 \times 10^{-11}$
Feed flow rate (2)	0.88	0.92	0.44	0.46	0.36
1by2	-3.08	0.92	-1.54	0.46	$6.45 \times 10^{-3}$
<b>Caffeine</b>					
Mean	186.30	2.58	186.30	2.58	$4.55 \times 10^{-16}$
Temperature (1)	154.95	5.78	77.47	2.89	$2.25 \times 10^{-11}$
Feed flow rate (2)	6.84	5.78	3.42	2.89	0.26
1by2	-18.11	5.78	-9.06	2.89	$9.49 \times 10^{-3}$
<b>Chlorogenic acid</b>					
Mean	243.04	1.70	243.04	1.70	$2.45 \times 10^{-19}$
Temperature (1)	198.13	3.80	99.07	1.90	$1.14 \times 10^{-14}$
Feed flow rate (2)	6.40	3.80	3.20	1.90	0.12
1by2	-20.89	3.80	-10.45	1.90	$1.87 \times 10^{-4}$
<b>Caffeic acid</b>					
Mean	107.46	0.59	107.46	0.59	$1.57 \times 10^{-20}$
Temperature (1)	90.08	1.31	45.04	0.65	$7.53 \times 10^{-1}$
Feed flow rate (2)	2.79	1.31	1.40	0.65	0.06
1by2	-9.23	1.31	-4.62	0.65	$2.10 \times 10^{-5}$
<b>Rutin</b>					
Mean	81.97	1.00	81.97	1.00	$1.57 \times 10^{-20}$
Temperature (1)	84.59	2.25	42.30	1.12	$7.53 \times 10^{-1}$
Feed flow rate (2)	3.22	2.25	1.61	1.12	0.06
1by2	-8.51	2.25	-4.26	1.12	$2.10 \times 10^{-5}$
<b>Quercetin</b>					
Mean	0.68	$3.53 \times 10^{-3}$	0.68	$3.53 \times 10^{-3}$	$8.78 \times 10^{-21}$
Temperature (1)	0.37	$7.99 \times 10^{-3}$	0.19	$3.94 \times 10^{-3}$	$4.95 \times 10^{-14}$
Feed flow rate (2)	$4.70 \times 10^{-2}$	$7.99 \times 10^{-3}$	$2.37 \times 10^{-2}$	$3.94 \times 10^{-3}$	$8.88 \times 10^{-5}$
1by2	$-8.37 \times 10^{-2}$	$7.99 \times 10^{-3}$	$-4.19 \times 10^{-2}$	$3.94 \times 10^{-3}$	$4.05 \times 10^{-7}$

\*: Analysis of Variance (ANOVA) for the cumulative concentration of bioactive compounds obtained from the packed-bed extraction process after 60 min.

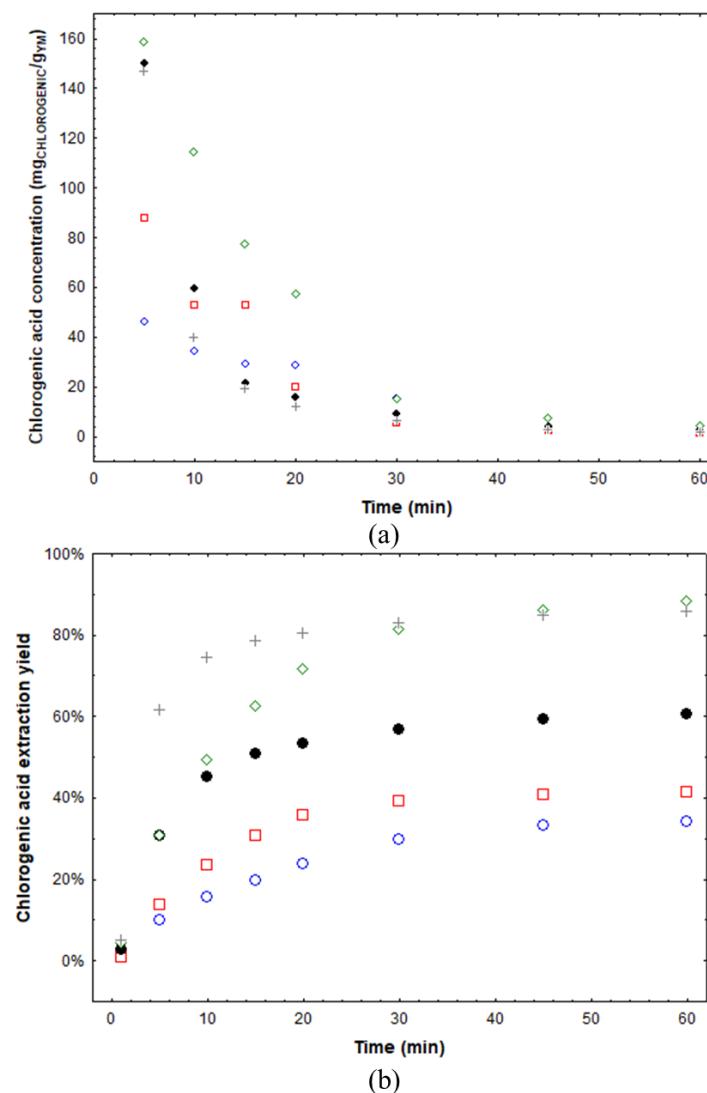
\*\*: Significant at  $p < 0.05$ .



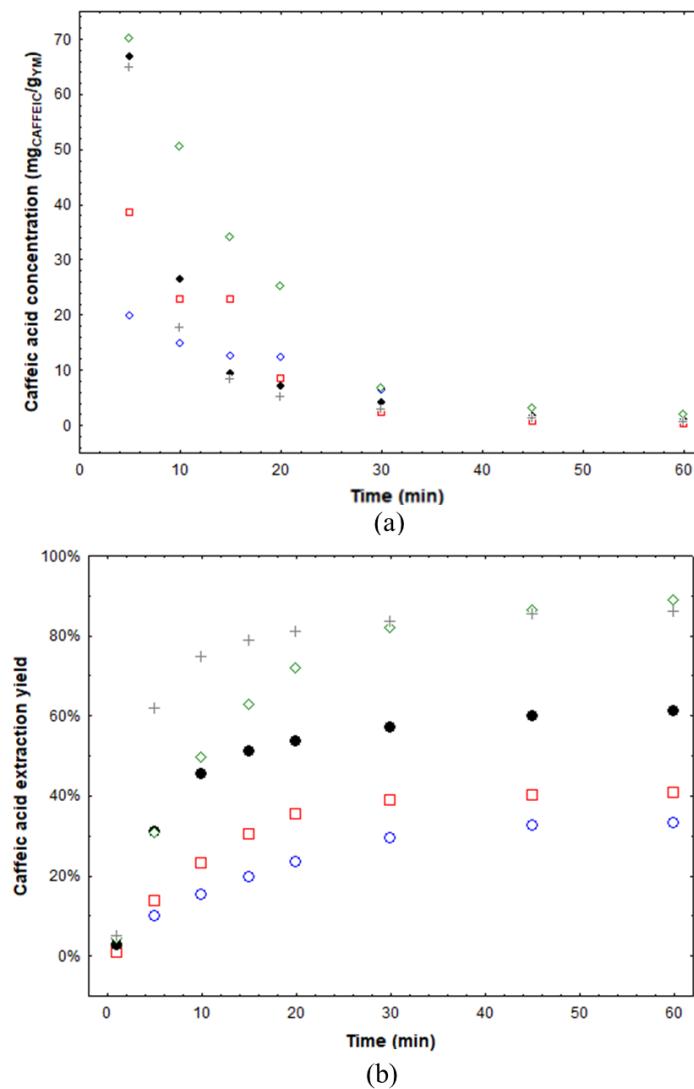
**Figure S1.** Kinetic of packed-bed extraction process for thebromine. (a) Theobromine concentration, (b) Theobromine extraction yield.  $\circ$   $T = 50^\circ\text{C}, Q = 20 \text{ cm}^3/\text{min}$ ;  $\square$   $T = 50^\circ\text{C}, Q = 20 \text{ cm}^3/\text{min}$ ;  $\bullet$   $T = 60^\circ\text{C}, Q = 15 \text{ cm}^3/\text{min}$ ;  $\lozenge$   $T = 70^\circ\text{C}, Q = 10 \text{ cm}^3/\text{min}$ ;  $+$   $T = 70^\circ\text{C}, Q = 20 \text{ cm}^3/\text{min}$ .



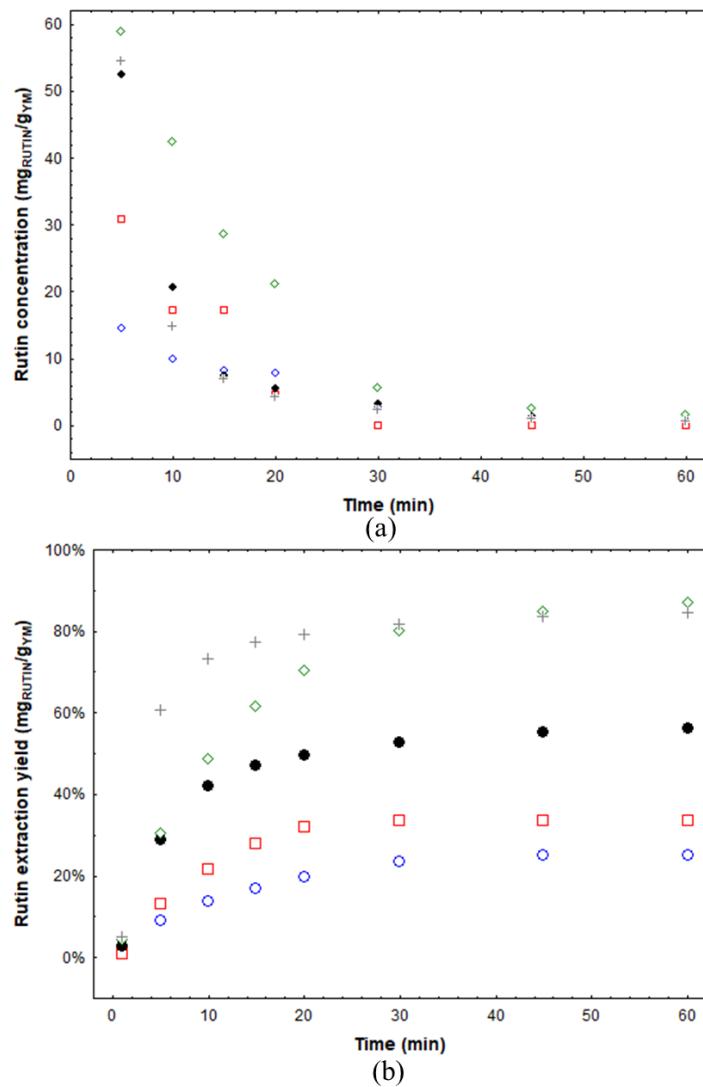
**Figure S2.** Kinetic of packed-bed extraction process for caffeine. (a) Caffeine concentration, (b) Caffeine extraction yield.  $\circ$   $T = 50^{\circ}\text{C}$ ,  $Q = 20 \text{ cm}^3/\text{min}$ ;  $\square$   $T = 50^{\circ}\text{C}$ ,  $Q = 20 \text{ cm}^3/\text{min}$ ;  $\bullet$   $T = 60^{\circ}\text{C}$ ,  $Q = 15 \text{ cm}^3/\text{min}$ ;  $\lozenge$   $T = 70^{\circ}\text{C}$ ,  $Q = 10 \text{ cm}^3/\text{min}$ ;  $+$   $T = 70^{\circ}\text{C}$ ,  $Q = 20 \text{ cm}^3/\text{min}$ .



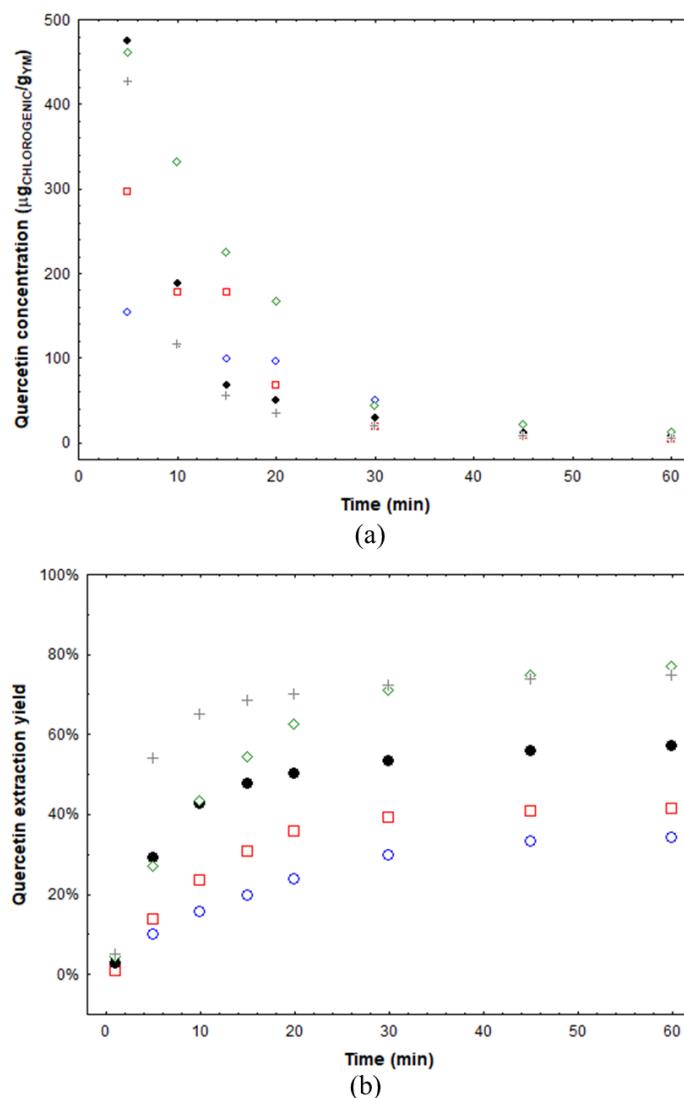
**Figure S3.** Kinetic of packed-bed extraction process for chlorogenic acid. (a) Chlorogenic acid, (b) Chlorogenic acid extraction yield.  $\circ$  T = 50 °C, Q = 20 cm<sup>3</sup>/min;  $\square$  T = 50 °C, Q = 20 cm<sup>3</sup>/min;  $\bullet$  T = 60 °C, Q = 15 cm<sup>3</sup>/min;  $\lozenge$  T = 70 °C, Q = 10 cm<sup>3</sup>/min;  $+$  T = 70 °C, Q = 20 cm<sup>3</sup>/min.



**Figure S4.** Kinetic of packed-bed extraction process for caffeic acid. (a) Caffeic acid concentration, (b) Caffeic acid extraction yield.  $\circ$  T = 50 °C, Q = 20 cm<sup>3</sup>/min;  $\square$  T = 50 °C, Q = 20 cm<sup>3</sup>/min;  $\bullet$  T = 60 °C, Q = 15 cm<sup>3</sup>/min;  $\lozenge$  T = 70 °C, Q = 10 cm<sup>3</sup>/min;  $+$  T = 70 °C, Q = 20 cm<sup>3</sup>/min.



**Figure S5.** Kinetic of packed-bed extraction process for rutin. (a) Rutin concentration, (b) Rutin extraction yield.  $\text{O} \quad T = 50^\circ\text{C}, Q = 20 \text{ cm}^3/\text{min}$ ;  $\square \quad T = 50^\circ\text{C}, Q = 20 \text{ cm}^3/\text{min}$ ;  $\bullet \quad T = 60^\circ\text{C}, Q = 15 \text{ cm}^3/\text{min}$ ;  $\diamond \quad T = 70^\circ\text{C}, Q = 10 \text{ cm}^3/\text{min}$ ;  $+$   $T = 70^\circ\text{C}, Q = 20 \text{ cm}^3/\text{min}$ .



**Figure S6.** Kinetic of packed-bed extraction process for quercitin. (a) Quercitin concentration, (b) Quercitin extraction yield.  $\textcircled{O}$  T = 50 °C, Q = 20 cm<sup>3</sup>/min;  $\square$  T = 50 °C, Q = 20 cm<sup>3</sup>/min;  $\bullet$  T = 60 °C, Q = 15 cm<sup>3</sup>/min;  $\lozenge$  T = 70 °C, Q = 10 cm<sup>3</sup>/min;  $+$  T = 70 °C, Q = 20 cm<sup>3</sup>/min.

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